



Numerical Topology Optimization of Heat Sinks

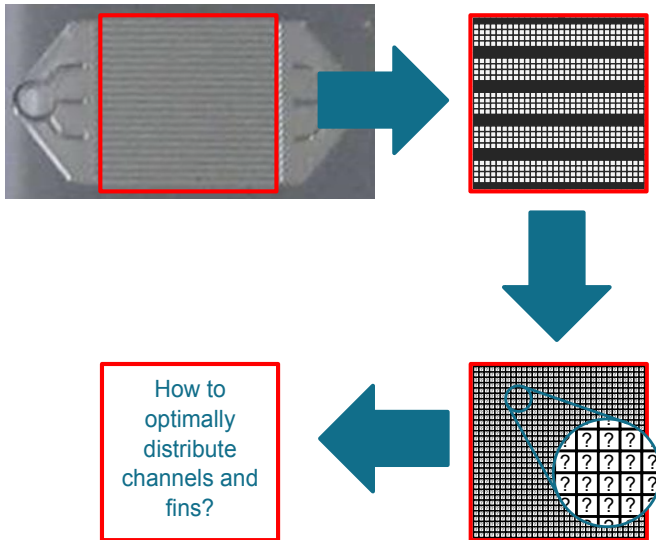
IHTC-15 Conference (Kyoto, Japan)

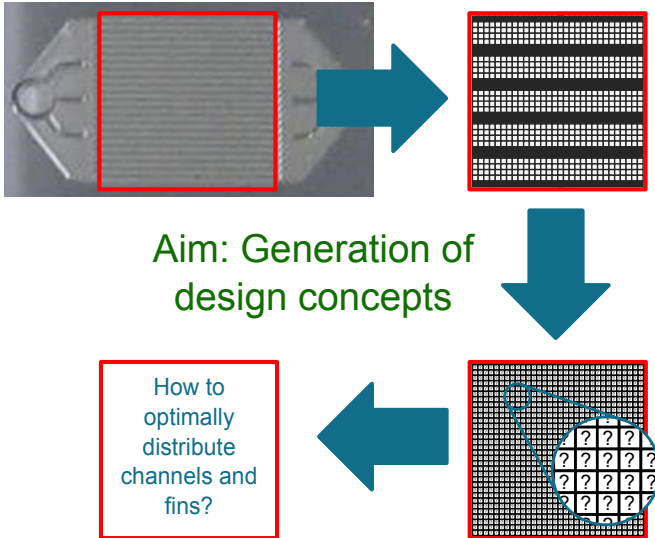
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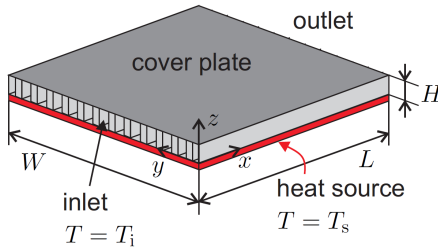
August 15, 2014



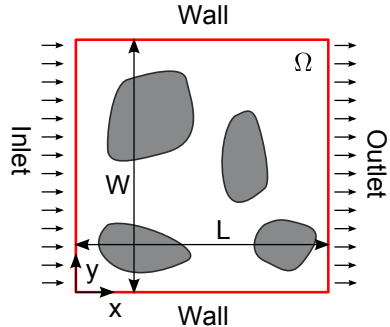


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- 2 Modelling and parametrization for topology optimization
- 3 Optimization method
- 4 Micro heat sink application
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(a) 3D heat sink



(b) 2D heat sink

- Simulation of heat sink state $\phi(\mathbf{x})$ from porosity distribution $\varepsilon(\mathbf{x})$ based on two-dimensional model ($\phi = [\mathbf{v}, p, T]^T$)
- Vertical profiles corresponding to fully developed flow through parallel plates

Field equations $\mathbf{M}(\varepsilon, \phi) = 0$:

- **Hybrid**: apply to *solid and fluid regions* by **controlling parameters**
- Averaged over height $\langle \cdot \rangle$: *2D simplification*

$$\nabla \cdot \langle \mathbf{v} \rangle = 0 \quad (\text{Continuity})$$

$$\nabla \cdot [K_c^m] \rho \langle \mathbf{v} \rangle \langle \mathbf{v} \rangle - \nabla \cdot \mu \nabla \langle \mathbf{v} \rangle + \nabla \langle p \rangle + [\alpha] \langle \mathbf{v} \rangle = 0 \quad (\text{Momentum})$$

$$\nabla \cdot [K_c^e] \rho c \langle T \rangle \langle \mathbf{v} \rangle - \nabla \cdot k \nabla \langle T \rangle + \underbrace{k \frac{K_d^e}{H^2} (\langle T \rangle - T_s)}_{\text{source heat flux}} = 0 \quad (\text{Energy})$$

Control parameters:

- Fluid: $\kappa = \infty$ & $k = k_f$
- Solid: $\kappa = 0$ & $k = k_s$

Averaging parameters:

- $K_c^m = 1.2$, $K_d^m = 12$,
 $K_c^e = 1.057$, $K_d^e = 2.569$
- $\alpha = \mu \left(\frac{1}{\kappa} + \frac{K_d^m}{H^2} \right)$

Porosity distribution $\varepsilon(\mathbf{x})$:



Solid material ($\varepsilon = 0$)



Cooling fluid ($\varepsilon = 1$)

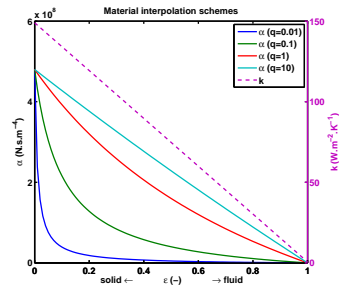
Mapping of physical parameters:

- Momentum loss coefficient α ('inverse permeability'):

$$\varepsilon \mapsto \alpha_q(\varepsilon) = \alpha_{\max} + (\alpha_{\min} - \alpha_{\max}) \varepsilon \frac{1+q}{\varepsilon+q} \quad (*)$$

- Heat conductivity k :

$$\varepsilon \mapsto k(\varepsilon) = k_s + (k_f - k_s) \varepsilon$$



(*) Borrvall, Petersson (2003), "Topology optimization of fluids in Stokes flow"

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For a general cost functional: $\mathcal{J}(\varepsilon, \phi) = \int_{\Omega} f d\mathbf{x} + \int_{\partial\Omega} g ds$

Adjoint equations $\mathbf{M}_{\phi}^*(\varepsilon, \phi)\phi^* = \nabla_{\phi}\mathcal{J}$:

$$\begin{aligned} -\nabla \cdot \mathbf{v}^* &= \frac{\partial f}{\partial p} \\ -K_c^m \rho \mathbf{v} \cdot (\nabla \mathbf{v}^* + (\nabla \mathbf{v}^*)^T) - \nabla \cdot \mu \nabla \mathbf{v}^* - \nabla p^* + \alpha \mathbf{v}^* + K_c^e \rho c T^* \nabla T &= \frac{\partial f}{\partial \mathbf{v}} \\ -K_c^e \rho c \mathbf{v} \cdot \nabla T^* - \nabla \cdot k \nabla T^* + k \frac{K_d^e}{H^2} T^* &= \frac{\partial f}{\partial T} \end{aligned}$$

Gradient of reduced cost functional $\hat{\mathcal{J}}(\varepsilon) = \mathcal{J}(\varepsilon, \phi(\varepsilon))$:

$$\nabla_{\varepsilon} \hat{\mathcal{J}}_{\varepsilon} = \left[\frac{\partial f}{\partial \varepsilon} \right] - \left[\frac{\partial \alpha}{\partial \varepsilon} \right] \mathbf{v} \cdot \mathbf{v}^* - \left[\frac{\partial k}{\partial \varepsilon} \right] \left(\nabla T \cdot \nabla T^* + \frac{K_d^e}{H^2} (T - T_s) T^* \right)$$

Maximization of total heat transfer rate:

$$\mathcal{J}(\varepsilon, \phi) = \int_A \dot{Q}'' dA = \int_{\Omega} k(\varepsilon) \frac{K_d^e}{H^2} (T_s - T) d\mathbf{x}$$

Implementation:

- FVM solver on Cartesian, structured grid
- Forward model $\mathbf{M}(\varepsilon, \phi) = 0$:
 - ① Coupled flow system (laminar)
 - ② Energy equation
- Adjoint model $\mathbf{M}_{\phi}^*(\varepsilon, \phi)\phi^* = \nabla_{\phi}\mathcal{J}$:
 - ① Adjoint energy equation
 - ② Coupled adjoint flow system
- Optimization with method of moving asymptotes (MMA):

Svanberg (1987), "The method of moving asymptotes — A new method for structural optimization"

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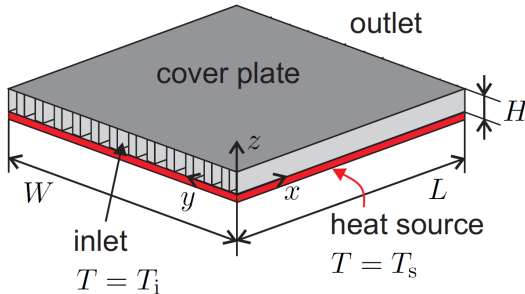
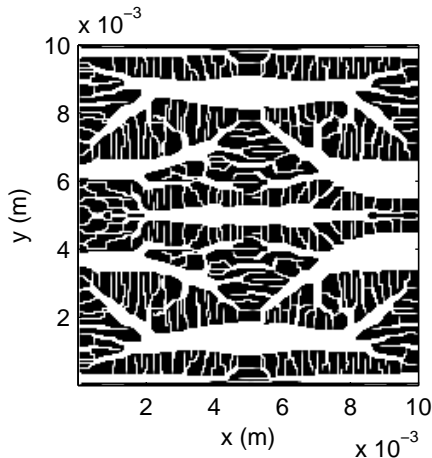


Figure: Maximizing total heat transfer rate of constant temperature heat source

Parameters

- Size: $L = W = 1\text{cm}$,
 $H = 500\mu\text{m}$
- Materials: Si, H_2O
- Pressure head: $\Delta p = 10\text{kPa}$
- Temperatures: $T_i = 0\text{K}$,
 $T_s = 40\text{K}$
- Stokes flow ($\text{Re} = 0$)
- $\alpha_{\min} = \mu \frac{K_d^m}{H^2}$, $\alpha_{\max} = \frac{K_d^m}{H^2}$
- $q_{\text{init}} = 0.01$, $q_{\text{final}} = 1$,
 $N_q = 50$, $N = 100$
- Grid size: 200×200

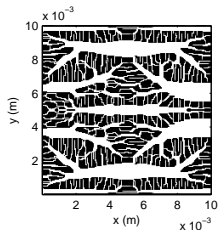


Realistic

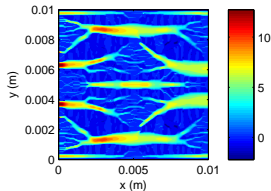
- Total heat transfer rate:
 $\dot{Q} = 794W$
- Several scales of channel diameters

R_{hs}	0.0504	K/W
\dot{m}	8.88	g/s
$\dot{m}c$	37.1	W/K
hA	28.4	W/K

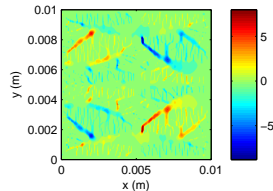
Figure: Porosity after 100 iterations



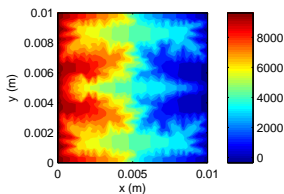
(a) Optimized design



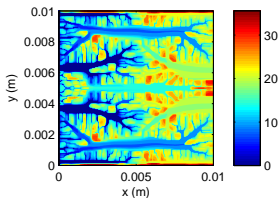
(b) Velocity (→) (m/s)



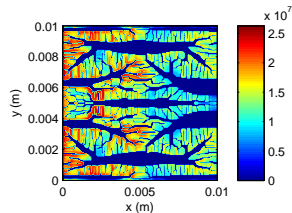
(c) Velocity (↑) (m/s)



(d) Pressure (Pa)



(e) Temperature (K)


(f) Source heat flux (W/m²)



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Conclusions

- Two-dimensional heat sink model for constant temperature heat source
- Pixel-based representation of geometries gives flexible parameterization, very suitable for topology optimization
- Continuous adjoint method efficiently calculates sensitivity
- Application on practical micro heat sink shows that topology optimization is very promising and powerful design method

Further work

- Tackle grid dependence: grid refinement generates finer heat sink structure
- Resolve dependency on α_{solid} and q

-  Van Oevelen T., Baelmans M. (2014), “Numerical topology optimization of heat sink” *IHTC-15 Conference, Kyoto, Japan*
-  Van Oevelen T., Baelmans M. (2014), “Application of topology optimization in a conjugate heat transfer problem” *OPT-i Conference, Kos, Greece*

THANK YOU!



Adjoint method applied to linearized model $\mathbf{M}_\phi(\varepsilon, \phi)\phi' + \mathbf{M}_\varepsilon(\varepsilon, \phi)\varepsilon' = 0$:

$$\int_{\Omega} \phi^* \cdot \mathbf{M}_\phi(\varepsilon, \phi)\phi' d\mathbf{x} = \int_{\Omega} \phi' \cdot \mathbf{M}_\phi^*(\varepsilon, \phi)\phi^* d\mathbf{x}$$

Derivative of reduced objective functional: $\hat{\mathcal{J}}(\varepsilon) = \mathcal{J}(\varepsilon, \phi(\varepsilon))$:

$$\begin{aligned} \frac{d\hat{\mathcal{J}}}{d\varepsilon}\varepsilon' &= \int_{\Omega} (\nabla_{\varepsilon}\mathcal{J}\varepsilon' + \nabla_{\phi}\mathcal{J}\phi') d\mathbf{x} &= \int_{\Omega} \left(\nabla_{\varepsilon}\mathcal{J} + \nabla_{\phi}\mathcal{J}\frac{\partial\phi}{\partial\varepsilon} \right) \varepsilon' d\mathbf{x} \\ &= \int_{\Omega} (\nabla_{\varepsilon}\mathcal{J}\varepsilon' + \phi^*\mathbf{M}_{\phi}\phi') d\mathbf{x} && (\mathbf{M}_{\phi}^*\phi^* = \nabla_{\phi}\mathcal{J}) \\ &= \int_{\Omega} \underbrace{(\nabla_{\varepsilon}\mathcal{J} - \mathbf{M}_{\varepsilon}^*\phi^*)}_{\nabla_{\varepsilon}\hat{\mathcal{J}}} \varepsilon' d\mathbf{x} && (\mathbf{M}_{\phi}\phi' = -\mathbf{M}_{\varepsilon}\varepsilon') \end{aligned}$$

$$\alpha_q(\varepsilon) = \alpha_{\max} + (\alpha_{\min} - \alpha_{\max}) \varepsilon \frac{1+q}{\varepsilon+q}$$

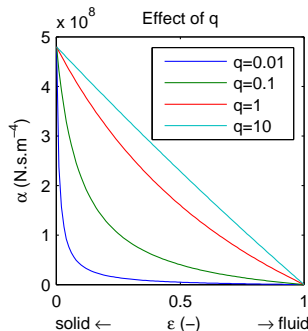
Updating procedure

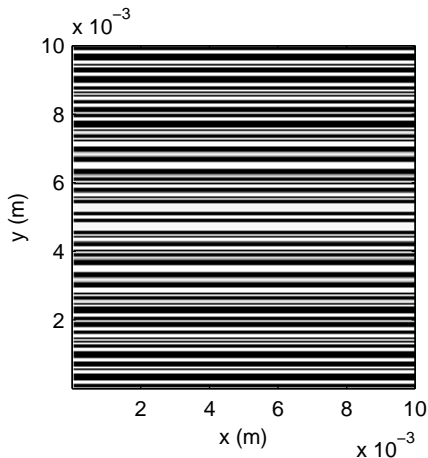
Set q_{init} , $q_{\text{final}} (> q_{\text{init}})$ and N_q :

$$q_1 = q_{\text{init}}, \quad \beta = \left(\frac{q_{\text{final}}}{q_{\text{init}}} \right)^{\frac{1}{N_q-1}}$$

For $k = 1, \dots, N_{\text{tot}}$, do:

$$q_{k+1} = \min(\beta q_k, q_{\text{final}})$$





Parallel microchannels

- Total heat transfer rate:
 $\dot{Q} = 347W$ ($\dot{Q} = 794W$)

R_{hs}	0.1152	0.0504	K/W
\dot{m}	3.91	8.88	g/s
$\dot{m}c$	16.3	37.1	W/K
hA	12.4	28.4	W/K

Unrestricted design

Figure: Porosity after 100 iterations

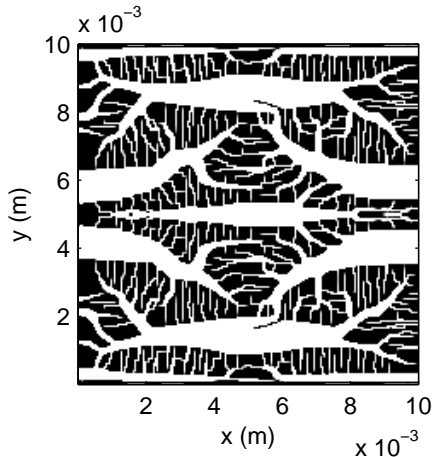


Figure: Porosity after 100 iterations

Unrealistic inlet conduction

- Total heat transfer rate:
 $\dot{Q} = 836W$
 - Advection outlet:
 $794W$
 - Conduction inlet:
 $41.4W$
- Cause: Inlet T b.c.
- Solution: Collector model
- *Quick fix: set $\varepsilon = 1$ in first cell*